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2nd Transnational Workshop
duratiNET
The Queen's University of Belfast
22nd June 2009

Carbonation, Chlorides & Electrochemical Repair

- Carbonation
- Chloride Attack
- Inspection & Testing
- Traditional Repair
- Electrochemical Repair
- Case Histories

The Problem

Millions of pounds are spent every year dealing with the symptoms of corrosion



Expense



Disruption

Danger

The Cause of the Problem

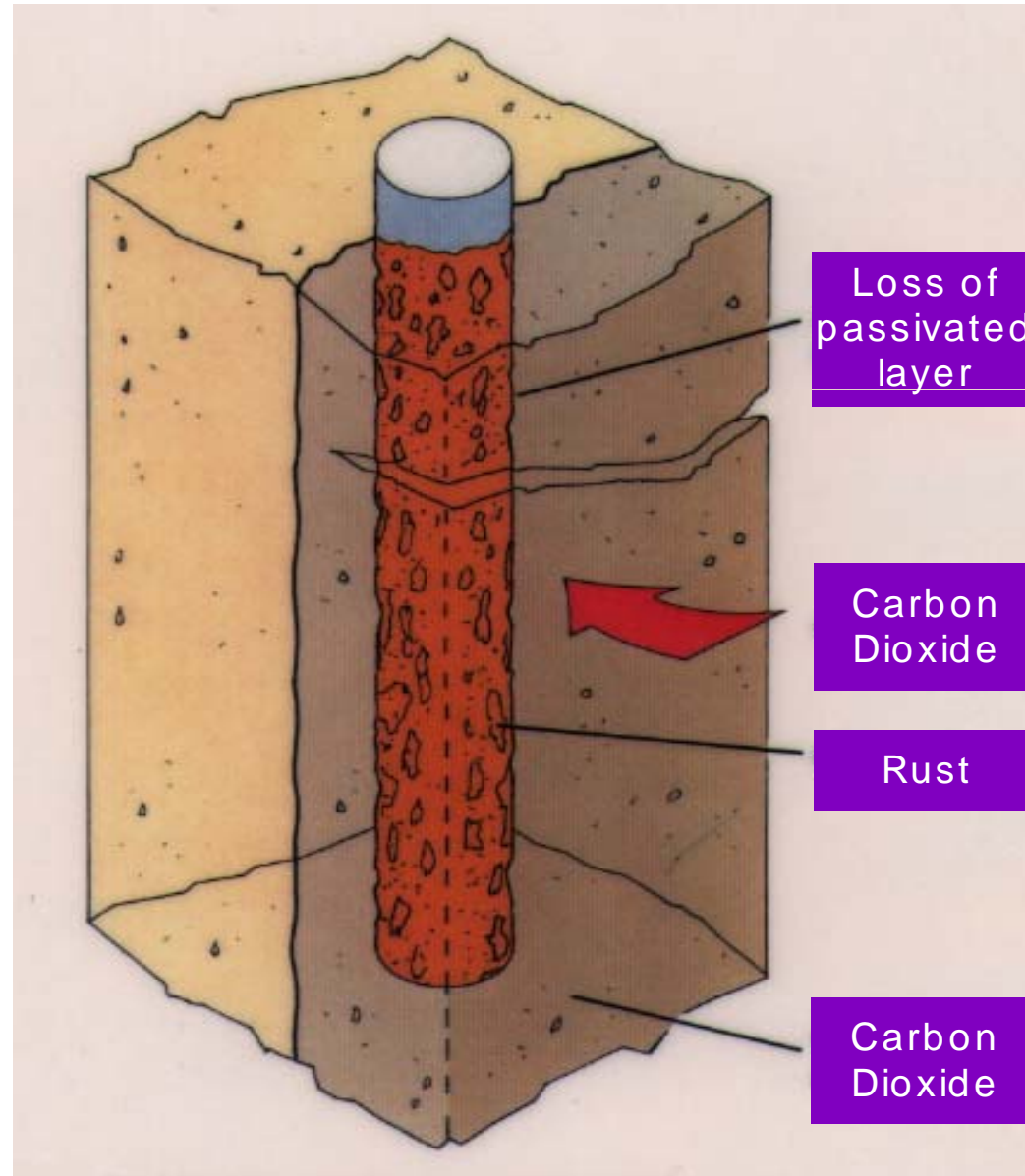


Poor design
Carbonation
ASR
Sulphate attack
Impact damage
Chemical attack

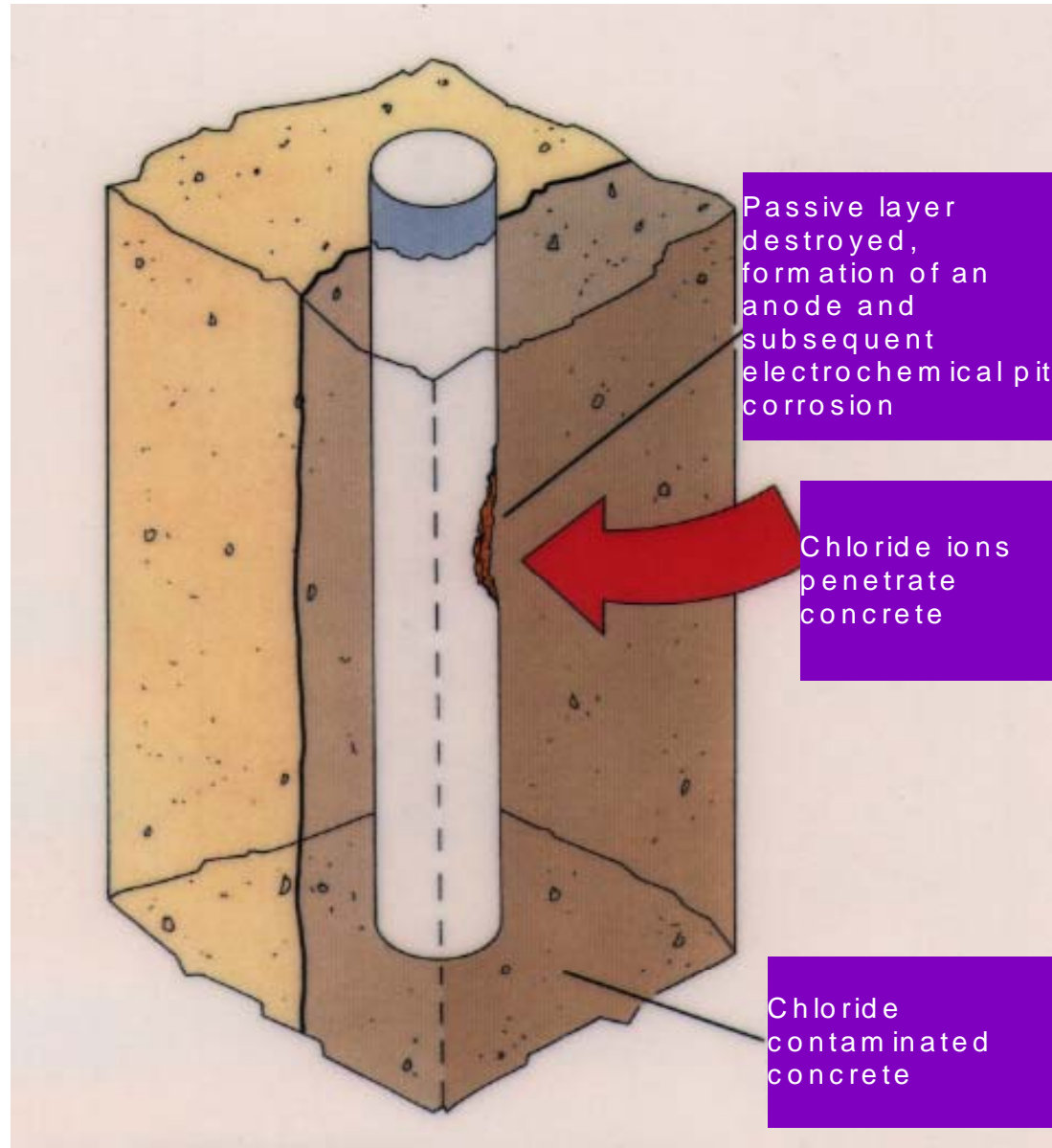


Chloride attack
Freeze thaw
Low cover
Poor site practice
Erosion

Carbonation



Chloride attack



Chloride induced corrosion pits





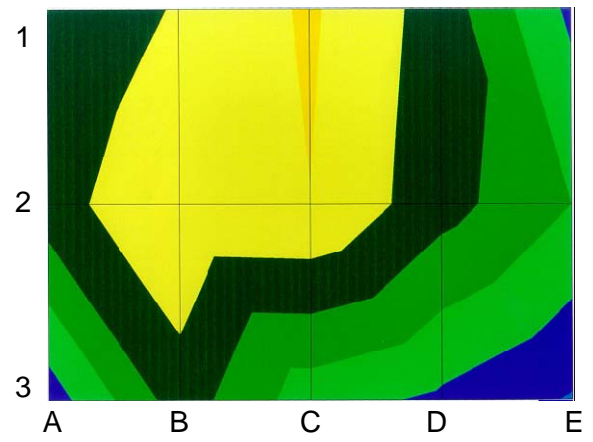
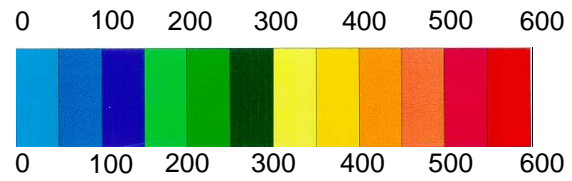
Chloride threshold values

Chloride content (% cement)	Risk of corrosion
< 0.4	Negligible
0.4 – 1.0	Possible
1.0 – 2.0	Probable
> 2.0	Certain

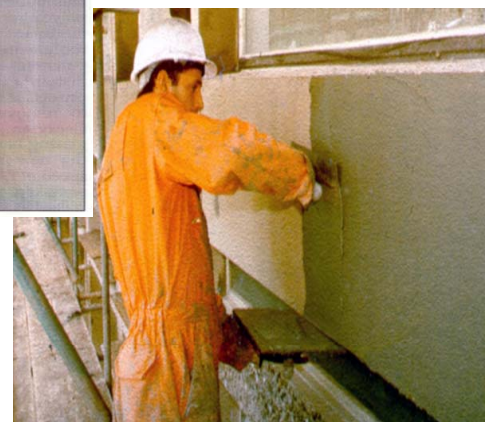
Ref: Browne (1982)

Half cell potential threshold values

CSE	Corrosion Condition
> -200 mV	Low – 10% risk of corrosion
-200 to -350 mV	Intermediate corrosion risk
< -350 mV	High - <90% risk of corrosion
< -500 mV	Severe corrosion



Traditional repair methods



BUT traditional patch repair alone does not

- Stop ongoing corrosion
- Prevent further spalling
- Break the repair cycle



Chasing the corrosion

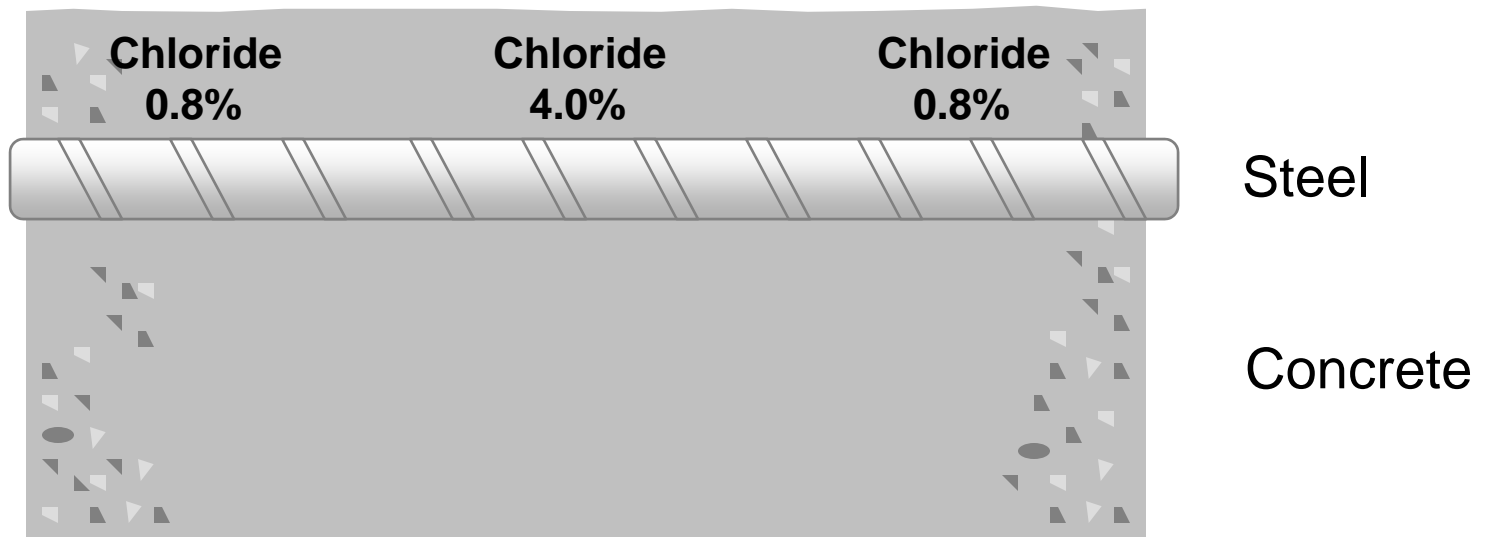


The problem ... “the newly established cathodic area within the repair will drive the new anode site in the contaminated region”

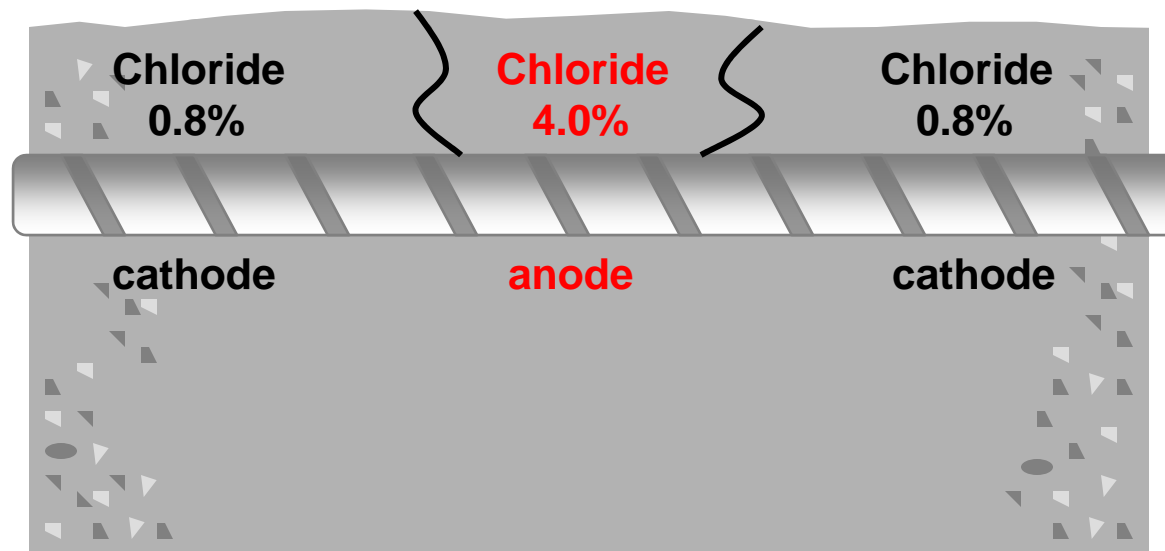


How does this mechanism work?

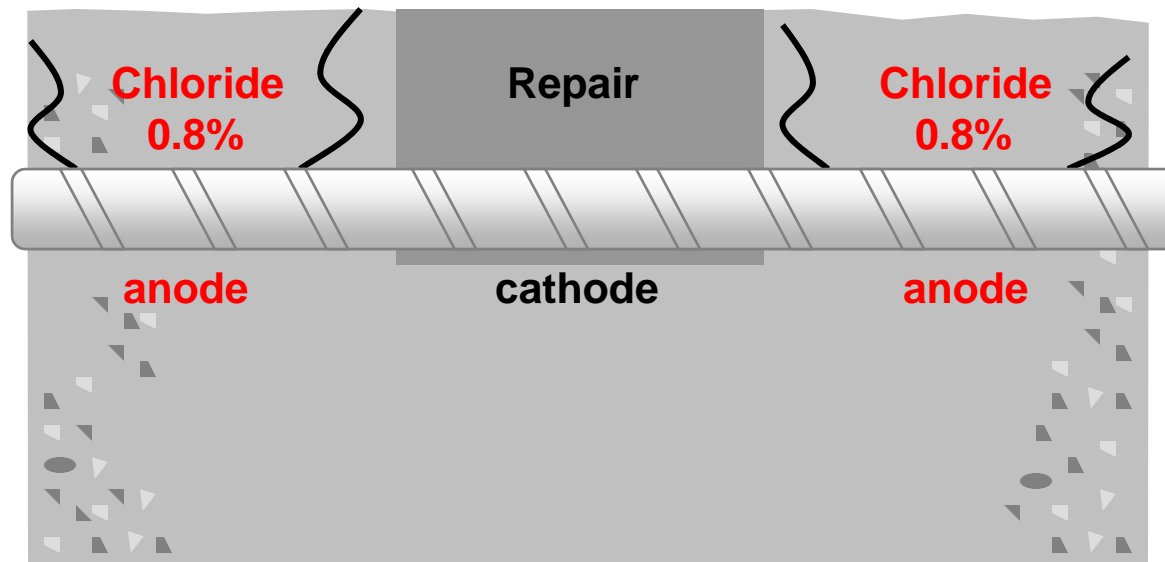
Chloride contaminated concrete prior to patch repair



Chloride contaminated concrete prior to patch repair



incipient anode effect



Downsides of Traditional Repair

Break out all contaminated concrete



Noisy

Expensive

Dusty

Disruptive

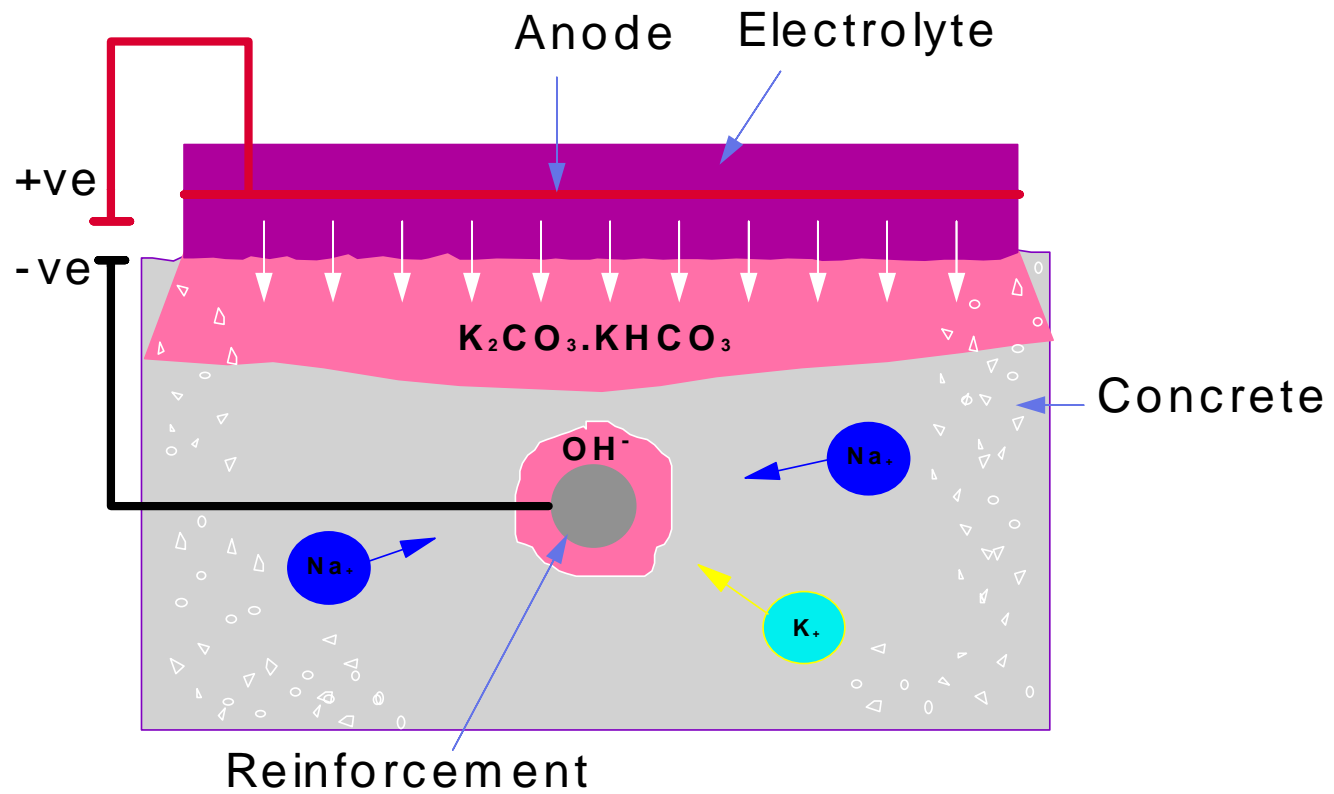
Electrochemical Repair

“Fighting Fire with Fire”

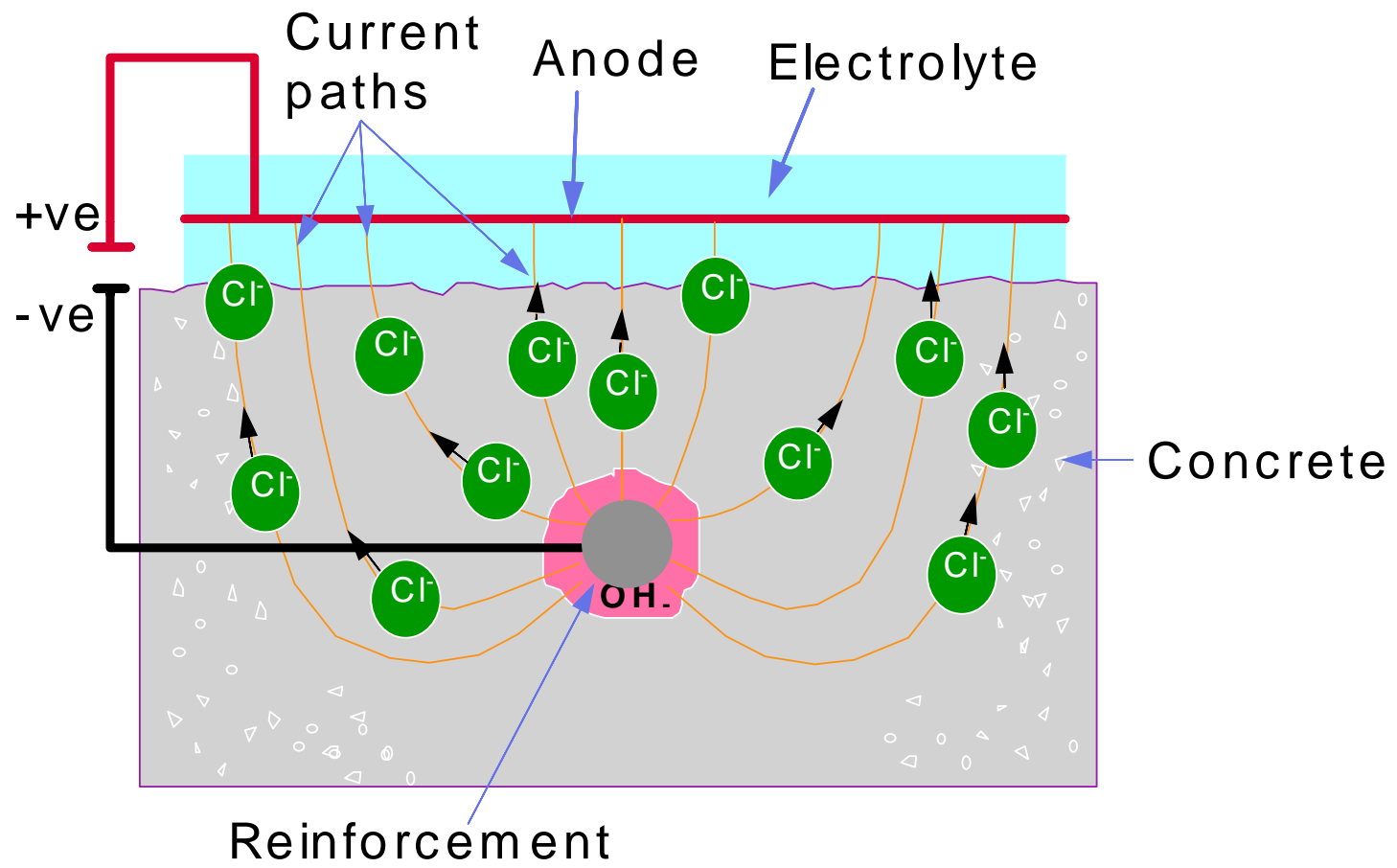
- **Cathodic Protection**
- **Realkalisation**
- **Chloride Extraction**
- **Sacrificial Anodes**
- **Next Generation Hybrid Systems**

Cathodic Protection





Chloride Extraction



Hydroxide Precipitation



XP



for patch repairs

CC



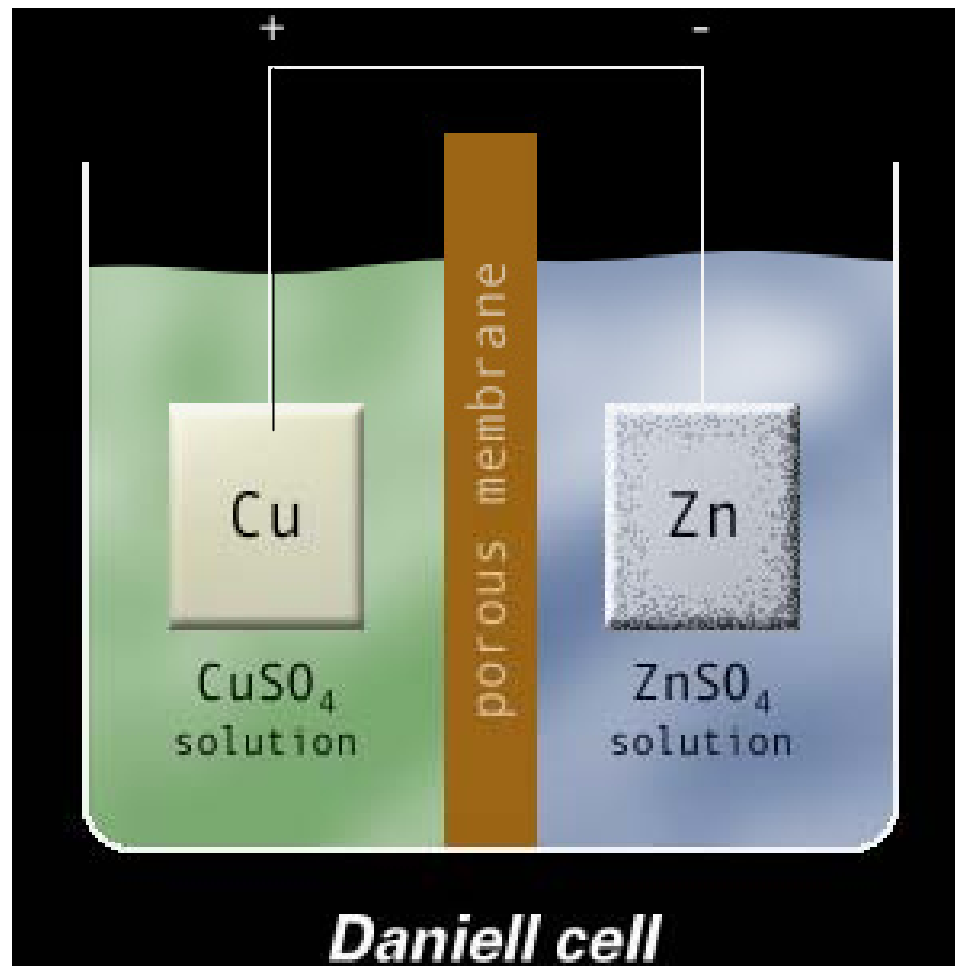
for blanket protection

LJ



for jetty piles

All the Galvashield systems work on the same principle ...



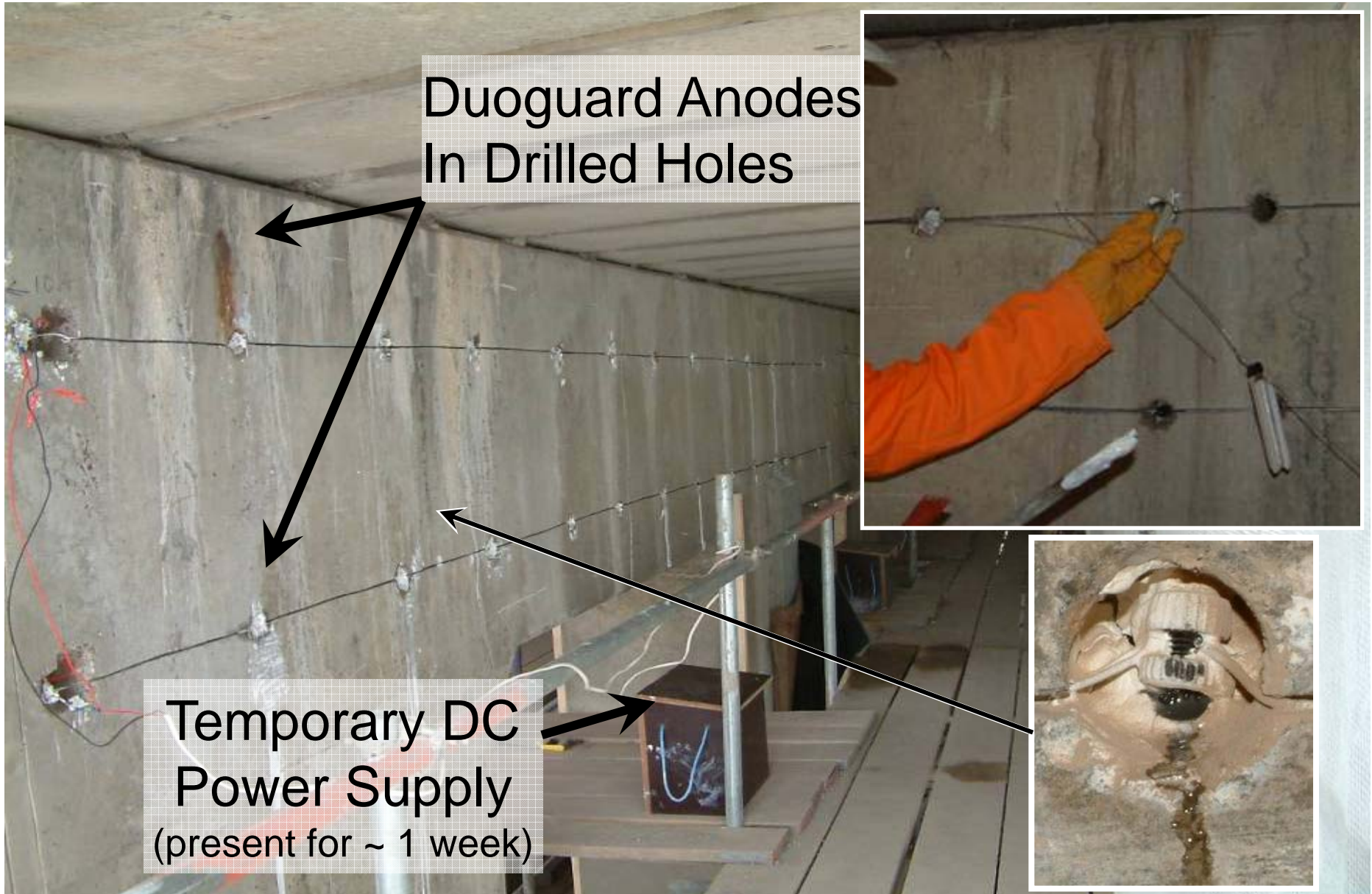
Oil Rig Example



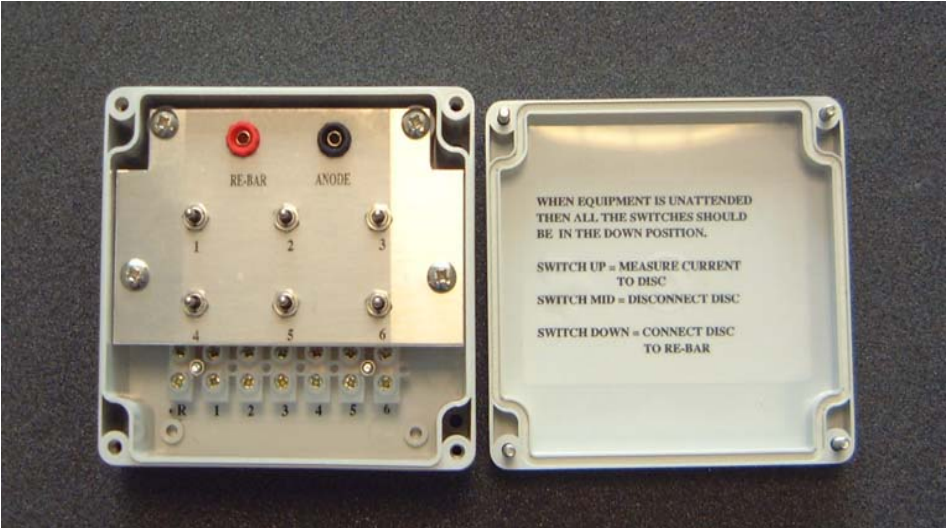
Photo Courtesy of Wilson Walton

- Chloride extraction type process
- Cathodic prevention type process (low maintenance)
- Single electrode system

- Install discrete alloy electrodes
- Apply specialised electrochemical treatment for 1 week
- Connect activated sacrificial anode to steel



Monitoring options



Manual monitoring box

Measure

Current ↙

Temperature ↙

Steel potential ↙

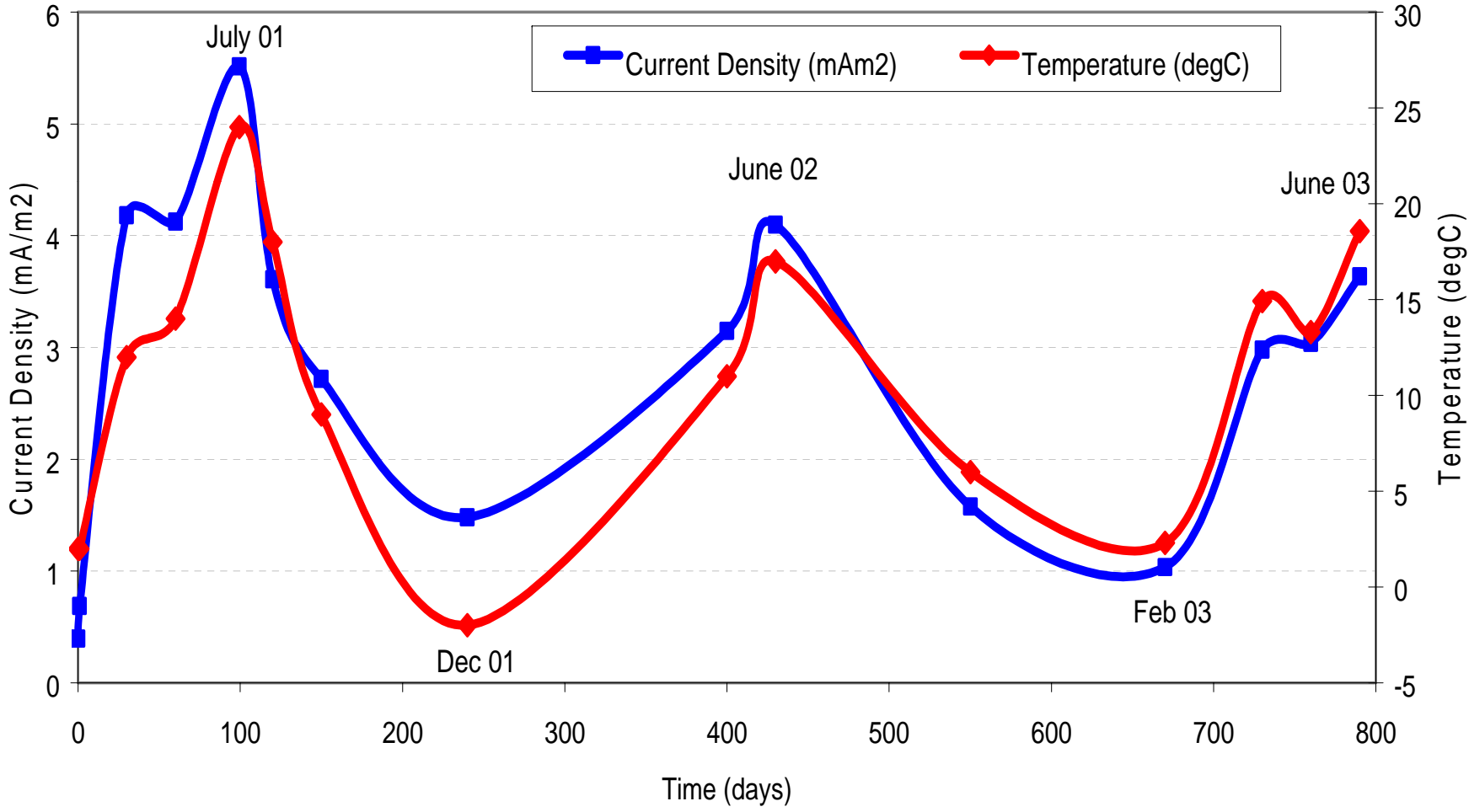
Residual life ↙



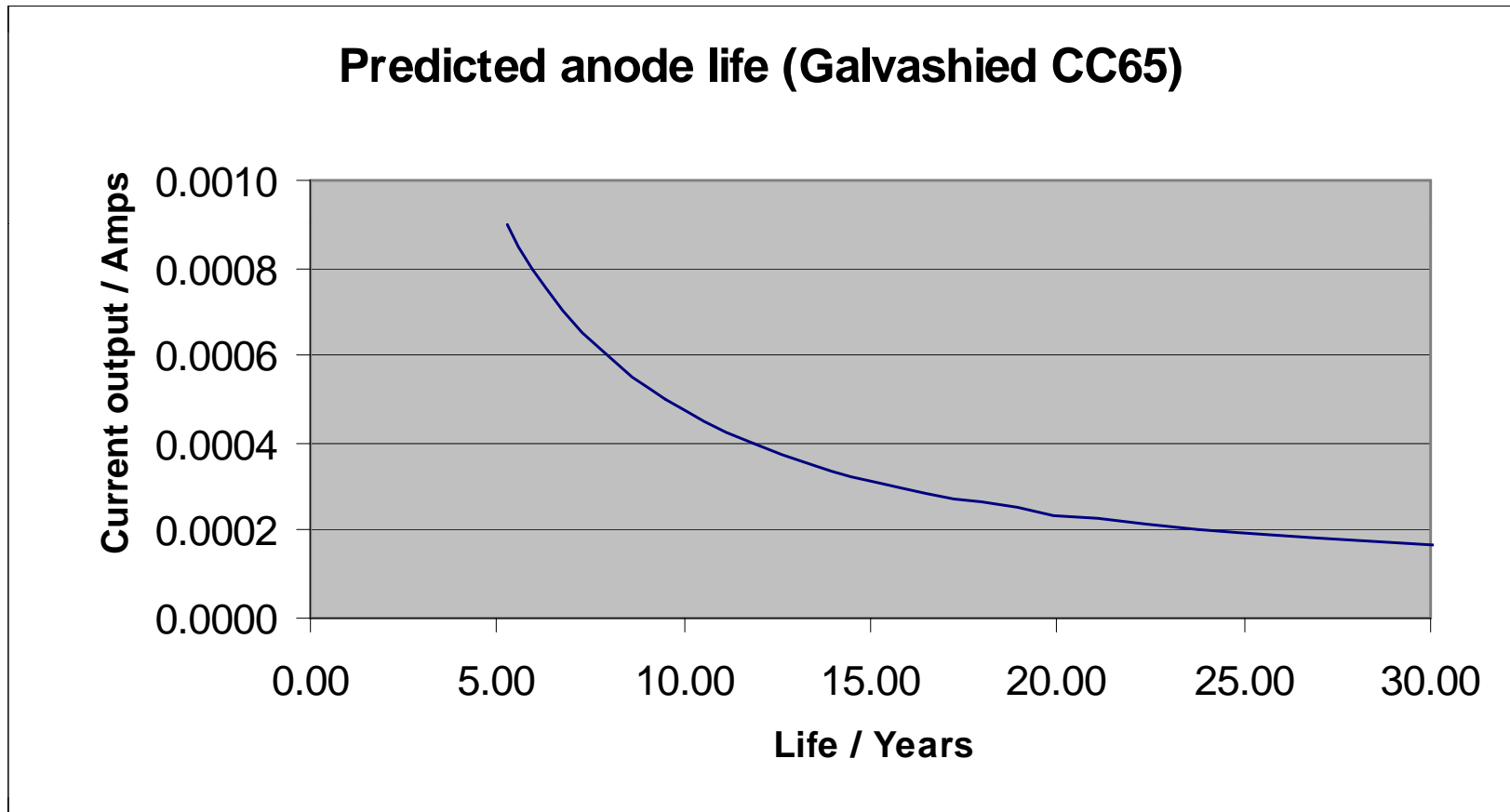
Automated monitoring box

Current output can be easily monitored

Eaton Park Pavillions, Norwich: CC anodes installed April 2001:Current Density results



Residual life can be calculated



Comber Bridge



Comber Bridge



Comber Bridge



Comber Bridge



Carrick Leisure Centre





Lakeland Forum





Eglinton Church





Red Arch Bridge



Red Arch Bridge



Red Arch Bridge



Ballylumford Jetty



Ballylumford Jetty



Beatties Bridge



Beatties Bridge



- **Carbonation & Chloride Attack are the main problems encountered**
- **Traditional Repair alone rarely deals with the source of the problem**
- **Electrochemical Repair treats “Fire with Fire” and deals with the source of the problem – reinforcement corrosion**
- **Realkalisation & Chloride Extraction are time consuming and costly**
- **Cathodic Protection requires a power source and monitoring and is prone to breaking down, vandalism and failure of the anodes**
- **Sacrificial Anodes are passive**
- **Hybrid Solutions maximise the benefits of CP, CE and SAs without the downsides**